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(54) **IMPROVED TREADWEAR/HYSTERESIS CARBON BLACKS.**

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- (73) Proprietor: **CABOT CORPORATION**
75 State Street
Boston, MA 02109 (US)
- (72) Inventor: **CHIUNG-HUEI, Shieh**
5 Philbrook Terrace
Lexington, MA 02173 (US)
Inventor: **BRANAN, John**
3815 Ozark
Amarillo, TX 79109 (US)
- (74) Representative: **von Kreisler, Alek,**
Dipl.-Chem. et al
Patentanwälte
von Kreisler-Selting-Werner
Postfach 10 22 41
D-50462 Köln (DE)

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Description

This application is a continuation-in-part of application Serial No. 07/492,894 filed March 13, 1990.

5 Field of the Invention

The present invention relates to a class of new and novel furnace carbon blacks which are suitable for various applications and particularly well suited for use in rubber compositions.

10 Background

Carbon blacks are generally produced in a furnace-type reactor by pyrolyzing a hydrocarbon feedstock with hot combustion gases to produce combustion products containing particulate carbon black.

Carbon blacks may be utilized as pigments, fillers, reinforcing agents and for a variety of other applications. For example, carbon blacks are widely utilized as fillers and reinforcing pigments in the
15 compounding and preparation of rubber compositions. Most importantly, carbon blacks are effective in the preparation of rubber vulcanizates intended for usage in preparing tires.

It is generally desirable in the production of tires to utilize carbon blacks which produce tires with satisfactory abrasion resistance and hysteresis performance. The treadwear properties of a tire are related
20 to abrasion resistance. The greater the abrasion resistance of a tire, the greater the number of miles the tire will last before wearing out. The hysteresis of a rubber compound means the difference between the energy applied to deform a rubber compound, and the energy released as the rubber compound recovers to its initial undeformed state. Tires with lower hysteresis values have reduced rolling resistance and heat build-up and therefore are able to reduce the fuel consumption of the vehicle utilizing the tire. Thus it is
25 particularly desirable to produce carbon blacks capable of imparting greater abrasion resistance and lower hysteresis to tires. Accordingly, one object of the present invention is the production of new carbon blacks which impart improved treadwear and hysteresis performance properties to natural rubbers, synthetic rubbers and blends of natural and synthetic rubbers incorporating the carbon blacks.

Another object of the present invention is new rubber compositions, advantageous for use as truck and
30 bus tires, incorporating the new carbon blacks.

Other objects of the present invention will become apparent from the following description and the claims.

Summary of the Invention

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We have discovered new carbon blacks having a CTAB of 120-160 m²/g (square meters per gram), a nitrogen surface area (N₂SA) of 125-180 m²/g, a CDBP (crushed dibutyl phthalate number) of 95-120 cc/100g, a DBP (dibutyl phthalate number) of 110-145 cc/100g, a Tint/CTAB ratio of 0.8-1.10, a ΔD50 of 70-100 and a ΔD50/Dmode ratio of 0.80-1.05. Preferably, the carbon blacks have a CTAB of 125-150 m²/g, a
40 N₂SA of 125-170 m²/g, a CDBP of 98-117 cc/100g, a DBP of 112-140 cc/100g, a Tint/CTAB ratio of 0.85-1.05, a ΔD50 of 72-90 and a ΔD50/Dmode ratio of 0.82-1.00. We have also discovered a new class of rubber compositions containing the carbon blacks.

The carbon blacks of the present invention may be produced in a furnace carbon black reactor having a first (combustion) zone, a transition zone, and a reaction zone. A carbon black yielding feedstock is injected
45 in any manner known to the art, into a hot combustion gas stream. The resultant mixture of hot combustion gases and feedstock passes into the reaction zone. Pyrolysis, of the carbon black yielding feedstock, is stopped by quenching the mixture when the carbon blacks of the present invention have been formed. Preferably pyrolysis is stopped by a quench injecting a quenching fluid. The process for preparing the novel carbon black of the present invention will be described in greater detail hereinafter.

The rubbers for which the novel carbon black of this invention are effective as reinforcing agents include natural and synthetic rubbers. Generally, amounts of the carbon black product ranging from 10 to 250 parts by weight can be used for each 100 parts by weight of rubber in order to impart a significant degree of reinforcement thereto. It is, however, preferred to use amounts varying from 20 to 100 parts by weight of carbon black per 100 parts by weight of rubber and especially preferred is the utilization of from
50 40 to 80 parts of carbon black per 100 parts of rubber.

Among the rubbers suitable for use with the present invention are natural rubber and its derivatives such as chlorinated rubber; copolymers of from 10 to 70 percent by weight of styrene and from 90 to 30 percent by weight of butadiene such as copolymer of 19 parts styrene and 81 parts butadiene, a copolymer

of 30 parts styrene and 70 parts butadiene, a copolymer of 43 parts styrene and 57 parts butadiene and a copolymer of 50 parts styrene and 50 parts butadiene; polymers and copolymers of conjugated dienes such as polybutadiene, polyisoprene, polychloroprene, and the like, and copolymers of such conjugated dienes with an ethylenic group-containing monomer copolymerizable therewith such as styrene, methyl styrene, chlorostyrene, acrylonitrile, 2-vinyl-pyridine, 5-methyl-2-vinylpyridine, 5-ethyl-2-vinylpyridine, 2-methyl-5-vinylpyridine, alkyl-substituted acrylates, vinyl ketone, methyl isopropenyl ketone, methyl vinyl ether, aliphatic carboxylic acids and the esters and amides thereof such as acrylic acid and dialkylacrylic acid amide; also suitable for use herein are copolymers of ethylene and other high alpha olefins such as propylene, butene-1 and pentene-1; particularly preferred are the ethylene-propylene copolymers wherein the ethylene content ranges from 20 to 90 percent by weight and also the ethylene-propylene polymers which additionally contain a third monomer such as dicyclopentadiene, 1,4-hexadiene and methylene norbornene.

An advantage of the carbon black of the present invention is that the carbon blacks impart greater abrasion resistance and lower hysteresis to compositions containing natural rubbers, synthetic rubbers or blends thereof in which the carbon blacks of the present invention are incorporated.

An advantage of the rubber compositions of the present invention is that the rubber compositions are particularly well suited for use as truck or bus tires with improved treadwear resistance and better fuel economy characteristics as compared to rubber compositions incorporating conventional, commercially available, carbon blacks.

Other advantages of the present invention will become apparent from the following more detailed description of the invention.

Brief Description of the Drawings:

Figure 1 is a cross-sectional view of a portion of one type of furnace carbon black reactor which may be utilized to produce the carbon blacks of the present invention.

Figure 2 is a graph of Rebound % versus Laboratory Abrasion Index at 7% Slip for rubber compositions produced with the carbon black of the present invention and for rubber compositions produced with reference carbon blacks.

Figure 3 is a graph of Rebound % versus Laboratory Abrasion Index at 14% Slip for rubber compositions produced with the carbon black of the present invention and for rubber compositions produced with reference carbon blacks.

Figure 4 is a graph of Rebound % versus Laboratory Abrasion Index at 21% Slip for rubber compositions produced with the carbon black of the present invention and for rubber compositions produced with reference carbon blacks.

Figure 5 is a sample histogram of the Stokes diameter of the aggregates of a carbon black sample versus the relative frequency of their occurrence in a given sample.

Detailed Description of the Invention:

The carbon black of the present invention is characterized by having a CTAB of 120-160 m²/g, a N₂SA of 125-180 m²/g, a CDBP of 95-120 cc/100g, a DBP of 110-145 cc/100g, a Tint/CTAB ratio of 0.80-1.10, a Δ D50 of 70-100 and a Δ D50/Dmode ratio of 0.80-1.05. Preferably, the carbon blacks have a CTAB of 125-150 m²/g, a N₂SA of 125-170 m²/g, a CDBP of 98-117 cc/100g, a DBP of 112-140 cc/100g, a Tint/CTAB ratio of 0.85-1.05, a Δ D50 of 72-90 and a Δ D50/Dmode ratio of 0.82-1.00.

The carbon blacks of the present invention may be produced in a modular, also referred to as "staged", furnace carbon black reactor. A section of a typical modular furnace carbon black reactor which may be utilized to produce the carbon black of the present invention is depicted in Figure 1. Other details of a typical modular furnace carbon black reactor may be found for example in the description contained in U.S. Patent No. 3,922,335, the disclosure of which is herein incorporated by reference.

Referring to Figure 1, the carbon blacks of the present invention may be produced in a furnace carbon black reactor 2, having a combustion zone 10, which has a zone of converging diameter 11, transition zone 12, and reaction zone 18. The diameter of the combustion zone 10, up to the point where the zone of converging diameter 11, begins is shown as D-1; the diameter of zone 12, as D-2; and the diameter of zone 18, as D-3. The length of the combustion zone 10, up to the point where the zone of converging diameter 11, begins is shown as L-1; the length of the zone of converging diameter is shown as L-2; and the length of the transition zone is shown as L-3.

To produce the carbon blacks of the present invention hot combustion gases are generated in combustion zone 10, by reacting a liquid or gaseous fuel with a suitable oxidant stream such as air, oxygen, mixtures of air and oxygen or the like. Among the fuels suitable for use in reacting with the oxidant stream in combustion zone 10, to generate the hot combustion gases are included any of the readily combustible gas, vapor or liquid streams such as natural gas, hydrogen, carbon monoxide, methane, acetylene, alcohols, or kerosene. It is generally preferred, however, to utilize fuels having a high content of carbon-containing components and in particular, hydrocarbons. The ratio of air to natural gas utilized to produce the carbon blacks of the present invention may be from 10:1 to 20:1. To facilitate the generation of hot combustion gases, the oxidant stream may be preheated.

The hot combustion gas stream flows downstream from zones 10 and 11 into zones 12 and then 18. The direction of the flow of hot combustion gases is shown in the figure by the arrow. Carbon black-yielding feedstock 30, is introduced at point 32 (located in zone 12). Carbon black-yielding feedstock 30, is simultaneously introduced upstream through probe 14 at point 34. The distance from the end of the zone of converging diameter 11, to point 32, is shown as F-1 and the distance from point 32 to upstream point 34 is shown as F-2. To produce the carbon black of the present invention, the feedstock may be injected in an amount of from 40% to 85%, by weight, at point 32, and the remainder of the total amount of from 15% to 60%, by weight, injected at point 34. Preferably from 50% to 65% of the total amount of feedstock, by weight, is introduced at point 32, and the remainder of the total amount of feedstock, from 35% to 50%, by weight, is introduced at point 34. In each of the examples described herein carbon black-yielding feedstock 30, was injected radially in the form of a plurality of jets which penetrate into the interior regions of the hot combustion gas stream to insure a high rate of mixing and shearing of the hot combustion gases and the carbon black-yielding feedstock so as to rapidly and completely decompose and convert the feedstock to the novel carbon black of the present invention.

The mixture of carbon black-yielding feedstock and hot combustion gases flows downstream through zone 12 into zone 18. Quench 40, located at point 42, injecting quenching fluid 50, which in Examples 1 - 4 is water, is utilized to stop pyrolysis of the carbon black-yielding feedstock when the novel carbon blacks of the present invention are formed. Point 42 may be determined in any manner known to the art, for selecting the position of a quench to stop pyrolysis. One method for determining the position of the quench to stop pyrolysis is by determining the point at which an acceptable toluene extract level for the novel carbon blacks of the present invention is achieved. Toluene extract level may be measured by using ASTM Test D1618-83 "Carbon Black Extractables - Toluene Discoloration". Q is the distance from the beginning of zone 18 to quench point 42, and will vary according to the position of the quench.

After the mixture of hot combustion gases and carbon black-yielding feedstock is quenched, the cooled gases pass downstream into any conventional cooling and separating means whereby the carbon blacks are recovered. The separation of the carbon black from the gas stream is readily accomplished by conventional means such as a precipitator, cyclone separator or bag filter. This separation may be followed by pelletizing using, for example, a wet pelletizer.

The following testing procedures are used in the determination and evaluation of the analytical properties of the carbon blacks of the present invention, and the physical properties of the rubber compositions incorporating the carbon blacks of the present invention.

CTAB of the carbon blacks was determined according to ASTM Test Procedure D3765-85. N₂SA of the carbon blacks was determined according to ASTM D3037-88. Tinting strength (Tint) of the carbon blacks was determined according to ASTM Test Procedure D3265-85a. The CDBP (Crushed Dibutyl Phthalate) of the carbon black pellets was determined according to the procedure set forth in ASTM D 3493-86. The DBP of the carbon black pellets was determined according to the procedure set forth in ASTM D2414.

Dmode, and ΔD_{50} of the carbon blacks were determined in the following manner. A histogram is made of the Stokes diameter of the aggregates of the carbon black sample versus the relative frequency of their occurrence in a given sample. As shown in Figure 5, a line (B) is drawn from the peak (A) of the histogram in a direction parallel to the Y axis to and ending at the X-axis at point (C) of the histogram. The midpoint (F) of the resultant line (B) is determined and a line (G) is drawn through the midpoint (F) thereof parallel to the X-axis. Line (G) intersects the distribution curve of the histogram at two points D and E. The absolute value of the difference of the two Stokes diameters of the carbon black particles at points D and E is the ΔD_{50} value.

The data used to generate the histogram are determined by the use of a disk centrifuge such as the one manufactured by Joyce Loebel Co. Ltd. of Tyne and Wear, United Kingdom. The following procedure is a modification of the procedure described in the instruction manual of the Joyce Loebel disk centrifuge file reference DCF 4.008 published on February 1, 1985, the teachings of which are hereby incorporated by reference, and was used in determining the data.

The procedure is as follows. 10 mg (milligrams) of a carbon black sample are weighed in a weighing vessel, then added to 50 cc of a solution of 10% absolute ethanol and 90% distilled water which is made 0.05% NONIDET P-40 surfactant (NONIDET P-40 is a registered trademark for a surfactant manufactured and sold by Shell Chemical Co.). The resulting suspension is dispersed by means of ultrasonic energy for 5 15 minutes using Sonifier Model No. W 385, manufactured and sold by Heat Systems Ultrasonics Inc., Farmingdale, New York.

Prior to the disk centrifuge run the following data are entered into the computer which records the data from the disk centrifuge:

1. The specific gravity of carbon black, taken as 1.86 g/cc;
- 10 2. The volume of the solution of the carbon black dispersed in a solution of water and ethanol, which in this instance is 0.5 cc.;
3. The volume of spin fluid, which in this instance is 10 cc of water;
4. The viscosity of the spin fluid, which in this instance is taken as 0.933 centipoise at 23 degrees C;
5. The density of the spin fluid, which in this instance is 0.9975 g/cc at 23 degrees C;
- 15 6. The disk speed, which in this instance is 8000 rpm;
7. The data sampling interval, which in this instance is 1 second.

The disk centrifuge is operated at 8000 rpm while the stroboscope is operating. 10 cc of distilled water are injected into the spinning disk as the spin fluid. The turbidity level is set to 0; and 1 cc of the solution of 10% absolute ethanol and 90% distilled water is injected as a buffer liquid. The cut and boost buttons of the 20 disk centrifuge are then operated to produce a smooth concentration gradient between the spin fluid and the buffer liquid and the gradient is monitored visually. When the gradient becomes smooth such that there is no distinguishable boundary between the two fluids, 0.5 cc of the dispersed carbon black in aqueous ethanol solution is injected into the spinning disk and data collection is started immediately. If streaming occurs the run is aborted. The disk is spun for 20 minutes following the injection of the dispersed carbon 25 black in aqueous ethanol solution. Following the 20 minutes of spinning, the disk is stopped, the temperature of the spin fluid is measured, and the average of the temperature of the spin fluid measured at the beginning of the run and the temperature of the spin fluid measured at the end of the run is entered into the computer which records the data from the disk centrifuge. The data is analyzed according to the standard Stokes equation and is presented using the following definitions:

30 Carbon black aggregate - a discrete, rigid colloidal entity that is the smallest dispersible unit; it is composed of extensively coalesced particles;

Stokes diameter - the diameter of a sphere which sediments in a viscous medium in a centrifugal or gravitational field according to the Stokes equation. A non-spherical object, such as a carbon black aggregate, may also be represented in terms of the Stokes diameter if it is considered as behaving as a 35 smooth, rigid sphere of the same density, and rate of sedimentation as the object. The customary units are expressed in nanometer diameters.

Mode (Dmode for reporting purposes) - The Stokes diameter at the point of the peak (Point A of Figure 5 herein) of the distribution curve for Stokes diameter.

Median Stokes diameter - (D_{st} for reporting purposes) the point on the distribution curve of Stokes 40 diameter where 50% by weight of the sample is either larger or smaller. It therefore represents the median value of the determination.

The Shore A Hardness of the rubber compositions was determined according to the procedure set forth in ASTM D-2240-86.

The abrasion data of the rubber compositions were determined using an abrader which is based on a 45 Lambourn type machine. Abrasion rates (cubic centimeter/centimeter travel) were measured at 7%, 13% and 21% slip. The slip is based on the relative velocity of the plates rather than angle of slip. In the following examples, the abrasion index is the ratio of the abrasion rate of a control composition containing VULCAN 6 carbon black, a trademarked product of Cabot Corporation, Waltham, Massachusetts divided by the abrasion rate of a composition produced using a specified carbon black of the present invention, at the 50 same slip.

The modulus, tensile and elongation of the rubber compositions were measured by the procedure set forth in ASTM D412.

Rebound data were determined on all rubber samples utilizing a ZWICK Rebound Resilience Tester, Model 5109, manufactured by Zwick of America, Inc., Post Office Box 997, East Windsor, Connecticut 55 06088. Instructions for determining the rebound values accompany the instrument.

The effectiveness and advantages of the present invention will be further illustrated by the following examples.

EXAMPLES 1-4

Four examples of the novel carbon blacks of the present invention were prepared in a reactor generally described herein, and as depicted in Figure 1, utilizing the reactor conditions and geometry set forth in Table I. The fuel utilized in the combustion reaction in each of the examples was natural gas. The liquid feedstock utilized in each of the examples had the properties indicated in the chart below:

	Feedstock Properties
Hydrogen/Carbon Ratio	0.93
Hydrogen (wt.%)	7.16
Carbon (wt.%)	91.2
Sulfur (wt.%)	0.4
A.P.I. Gravity 15.5/15.6 C(60)F [ASTM D-287]	-2.2
Specific Gravity 15.5/15.6 C(60)F [ASTM D-287]	1.094
Viscosity, SUS (54.4 °C) [ASTM D-88]	105.8
Viscosity, SUS (98.9 °C) [ASTM D-88]	40.8
BMCI (Visc-Grav)	135

The reactor conditions and geometry are set forth in Table I below.

TABLE I

		CARBON BLACKS			
		Ex. 1	Ex. 2	Ex. 3	Ex. 4
5	D-1, in.	7.25	7.25	7.25	7.25
	D-2, in.	5.3	5.3	5.3	5.3
	D-3, in.	9	9	9	9
10	L-1, in.	24	24	24	24
	L-2, in.	12	12	12	12
	L-3, in.	11.5	11.5	11.5	11.5
	F-1, in.	5.75	5.75	5.75	5.75
	F-2, in.	26	26	26	26
15	Q, in.	38	26	26	32
	Oil Inj Pt. 32,)	6 x	6 x	6 x	6 x
	Tips # x Size, in.)	0.031	0.0225	0.0225	0.0225
	Oil Rate 32, gph	93	94	85	94
	Oil Press. 32, psig	217	493	402	430
20	Oil Preheat, 32, °F	126	338	337	332
	Oil Inj. Pt. 34,)	3 x	3 x	3 x	3 x
	Tips # x Size, in.)	0.070	0.070	0.070	0.070
	Oil Rate 34, gph	46	46	43	47
	Oil Press. 34, psig	35	30	26	27
25	Oil Preheat 34, °F	224	267	256	257
	Comb.Air, kscfh	115	115	115	115
	Comb.Air Preheat, °F	900	900	900	900
	Natural Gas, kscfh	9.7	9.7	9.7	9.7
	Air/Burn Gas Ratio	9.9	9.9	9.9	9.9
30	K+, gK+/100gal oil	1.5	6.3	2.1	5.3
	Quench Press., psi	350	140	260	170
	Temp. at Quench, °F	1350	1350	1350	1350
35	Inj. = Injection; Comb. = combustion; Press. = pressure 32 = Point 32 on Figure 1; 34 = Point 34 on Figure 1; gph = gallons/hour; psi = pounds/square inch; in. = inches; ft. = feet; °F = degrees Fahrenheit; kscfh = standard cubic feet/hour, in 1000's K+ = potassium; gK+/100gal oil = grams K+/100 gallons feedstock (oil)				

40 The carbon blacks produced in Examples 1-4 were then analyzed according to the procedures described herein. The analytical properties of the blacks produced, after wet pelletizing and drying, and two reference carbon blacks were as follows:

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	Carbon Black					
	Ex.1	Ex.2	Ex.3	Ex.4	VULCAN 6	VULCAN 10H
CTAB (m ² /g)	131	129	149	135	109	135
N ₂ SA (m ² /g)	141	133	159	156	111	140
DBP (cc/100g)	118	114	128	115	114	127
CDBP (cc/100g)	104	100	110	102	98	102
Tint (%)	132	132	131	135	114	132
Tint/CTAB	1.01	1.02	0.88	1.00	1.04	0.98
Dmode	90	86	90	84	89	73
ΔD50	86	78	82	74	62	60
ΔD50/Dmode	0.96	0.91	0.87	0.84	0.70	0.82
VULCAN 6 carbon black and VULCAN 10H carbon black are trademarked carbon blacks manufactured and sold by Cabot Corporation, Waltham, Massachusetts.						

Example 5

This Example illustrates the use of the novel carbon blacks of the present invention in rubber compositions in comparison with rubber compositions produced using, VULCAN 6 carbon black and VULCAN 10H carbon black. Rubber composition A was made with the carbon black of the present invention produced in Example 1. Rubber composition B was made with the carbon black of the present invention produced in Example 2. Rubber composition C was made with the carbon black of the present invention produced in Example 3. Rubber composition D was made with the carbon black of the present invention produced in Example 4. Rubber composition E was made with VULCAN 6 carbon black. Rubber composition F was made with VULCAN 10H carbon black. Rubber compositions A, B, C, D, E and F were prepared incorporating each of the carbon black samples according to the rubber formulation procedure shown below in Table II.

TABLE II

INGREDIENT	Part by weight
Natural Rubber	100
Carbon Black	50.00
Zinc Oxide	5.00
Circo Light Rubber Process Oil	5.00
Stearic Acid	3.00
Sunproof Improved	2.50
Santoflex 13	1.5
AgeRite Resin D	1.5
Santocure MOR	1.2
Sulfur	1.8
Circo Light Rubber Process Oil is a naphthenic Oil, ASTM D2226, Type 103; Sunproof Improved is a mixture of waxy materials used as a stabilizer; Santoflex 13 is n-(1,3-dimethylbutyl)-N'phenyl-p-phenylene-diamine; AgeRite Resin D is polymerized 1,2-dihydro-2,2,4 trimethylquinoline; Santocure MOR is 2(Morpholiniothio) benzothiazole.	

The static properties of these rubber compositions were then evaluated according to the ASTM procedures described herein. The results were as follows:

Rubber Composition	Modulus 300% El (psi)	Tensile (psi)	El _b * (%)	Shore A Hardness
A	1514	3832	571	65
B	1834	4176	556	58
C	1946	4229	568	59
D	1911	4515	566	57
E	1591	3882	567	60
F	1503	4017	610	67

*El_b = elongation at break;
psi = pounds/square inch

These results show that the static properties of the rubber compositions A, B, C and D produced with the carbon blacks of the present invention are comparable to those of rubber compositions E and F produced with reference carbon blacks.

The Laboratory Abrasion Index and Rebound % of each rubber composition were also evaluated as described herein. The results were as follows:

Rubber Composition	7% Slip	13% Slip	21% Slip	Rebound %
A	128.4	123.3	101	47.4
B	122.1	136.2	119.4	48.7
C	121.5	123.6	116.1	46.1
D	116.1	129.3	143.2	47.1
E	100	100	100	53.7
F	116.7	106.0	95.9	46.5

The laboratory abrasion index data show that rubber compositions A, B, C and D, containing the carbon blacks of the present invention, exhibit improved abrasion resistance/hysteresis performance properties compared with rubber compositions E and F incorporating the control carbon blacks. The improved abrasion/hysteresis performance properties of the rubber compositions containing the carbon blacks of the present invention, at 7%, 13% and 21% slip values are depicted graphically in Figures 2, 3 and 4.

It should be clearly understood that the forms of the present invention herein described are illustrative only and are not intended to limit the scope of the invention.

Claims

1. A carbon black having a CTAB of 120-160 m²/g, a N₂SA of 125-180 m²/g, a CDBP of 95-120 cc/100g, a DBP of 110-145 cc/100g, a Tint/CTAB ratio of 0.80-1.10, a ΔD50 of 70-100 nm and a ΔD50/Dmode ratio of 0.80-1.05.
2. The carbon black of claim 1 wherein the CTAB is 125-150 m²/g, the N₂SA is 125-170 m²/g, the CDBP is 98-117 cc/100g, the DBP is 112-140 cc/100g, the Tint/CTAB ratio is 0.85-1.05, the ΔD50 is 72-90 nm and the ΔD50/Dmode ratio is 0.82-1.00.
3. The carbon black of claim 1 wherein the CTAB is 131 m²/g, the N₂SA is 141 m²/g, the CDBP is 104 cc/100g, the DBP is 118 cc/100g, the Tint/CTAB ratio is 1.01, the ΔD50 is 86 nm and the ΔD50/Dmode ratio is 0.96.
4. The carbon black of claim 1 wherein the CTAB is 129 m²/g, the N₂SA is 133 m²/g, the CDBP is 100 cc/100g, the DBP is 114 cc/100g, the Tint/CTAB ratio is 1.02, the ΔD50 is 78 nm and the ΔD50/Dmode ratio is 0.91.
5. The carbon black of claim 1 wherein the CTAB is 149 m²/g, the N₂SA is 159 m²/g, the CDBP is 110 cc/100g, the DBP is 108 cc/100g, the Tint/CTAB ratio is 0.88, the ΔD50 is 82 nm and the ΔD50/Dmode ratio is 0.87.

6. The carbon black of claim 1 wherein the CTAB is 135 m²/g, the N₂SA is 156 m²/g, the CDBP is 102 cc/100g, the DBP is 115 cc/100g, the Tint/CTAB ratio is 1.00, the Δ D50 is 74 nm and the Δ D50/mode ratio is 0.84.
- 5 7. A rubber composition comprising 100 parts, by weight, of a rubber and from 10 to 250 parts, by weight, of a carbon black having a CTAB of 120-160 m²/g, a N₂SA of 125-180 m²/g, a CDBP of 95-120 cc/100g, a DBP of 110-145 cc/100g, a Tint/CTAB ratio of 0.80-1.10, a Δ D50 of 70-100 nm and a Δ D50/Dmode ratio of 0.80-1.05
- 10 8. The rubber composition of claim 7 wherein the CTAB of the carbon black is 125-150 m²/g, the N₂SA of the carbon black is 125-170 m²/g, the CDBP of the carbon black is 98-117 cc/100g, the DBP of the carbon black is 112-140 cc/100g, the Tint/CTAB ratio of the carbon black is 0.85-1.05, the Δ D50 of the carbon black is 72-90 nm and the Δ D50/Dmode ratio of the carbon black is 0.82-1.00.
- 15 9. The rubber composition of claim 7 wherein the rubber is natural rubber.
10. The rubber composition of claim 7 wherein the carbon black is present in an amount of from 50 to 100 parts, by weight, per 100 parts, by weight rubber.

20 Patentansprüche

1. Ruß mit einem CTAB von 120-160 m²/g, einem N₂SA von 125-180 m²/g, einem CDBP von 95-120 cm³/100 g, einem DBP von 110-145 cm³/100g, einem Farbton/CTAB-Verhältnis von 0,80-1,10, einem Δ D50 von 70-100 nm und einem Δ D50/D-Mode-Verhältnis von 0,80-1,05.
- 25 2. Ruß gemäß Anspruch 1, worin das CTAB 125-150 m²/g ist, das N₂SA 125-170 m²/g ist, das CDBP 98-117 cm³/100 g ist, das DBP 112-140 cm³/100 g ist, das Farbton/CTAB-Verhältnis 0,85-1,05 ist, das Δ D50 72-90 nm ist und das Δ D50/D-Mode-Verhältnis 0,82-1,00 ist.
- 30 3. Ruß gemäß Anspruch 1, worin das CTAB 131 m²/g ist, das N₂SA 141 m²/g ist, das CDBP 104 cm³/100 g ist, das DBP 118 cm³/100 g ist, das Farbton/CTAB-Verhältnis 1,01 ist, das Δ D50 86 nm ist und das Δ D50/D-Mode-Verhältnis 0,96 ist.
4. Ruß gemäß Anspruch 1, worin das CTAB 129 m²/g ist, das N₂SA 133 m²/g ist, das CDBP 100 cm³/100 g ist, das DBP 114 cm³/100 g ist, das Farbton/CTAB-Verhältnis 1,02 ist, das Δ D50 78 nm ist und das Δ D50/D-Mode-Verhältnis 0,91 ist.
- 35 5. Ruß gemäß Anspruch 1, worin das CTAB 149 m²/g ist, das N₂SA 159 m²/g ist, das CDBP 110 cm³/100 g ist, das DBP 108 cm³/100 g ist, das Farbton/CTAB-Verhältnis 0,88 ist, das Δ D50 82 nm ist und das Δ D50/D-Mode-Verhältnis 0,87 ist.
- 40 6. Ruß gemäß Anspruch 1, worin das CTAB 135 m²/g ist, das N₂SA 156 m²/g ist, das CDBP 102 cm³/100 g ist, das DBP 115 cm³/100 g ist, das Farbton/CTAB-Verhältnis 1,00 ist, das Δ D50 74 nm ist und das Δ D50/D-Mode-Verhältnis 0,84 ist.
- 45 7. Kautschuk-Zusammensetzung umfassend 100 Gewichtsteile eines Kautschuks und 10 bis 250 Gewichtsteile eines Rußes mit einem CTAB von 120-160 m²/g, einem N₂SA von 125-180 m²/g, einem CDBP von 95-120 cm³/100 g, einem DBP von 110-145 cm³/100g, einem Farbton/CTAB-Verhältnis von 0,80-1,10, einem Δ D50 von 70-100 nm und einem Δ D50/D-Mode-Verhältnis von 0,80-1,05.
- 50 8. Kautschuk-Zusammensetzung gemäß Anspruch 7, worin das CTAB des Rußes 125-150 m²/g ist, das N₂SA des Rußes 125-170 m²/g ist, das CDBP des Rußes 98-117 cm³/100 g ist, das DBP des Rußes 112-140 cm³/100 g ist, das Farbton/CTAB-Verhältnis des Rußes 0,85-1,05 ist, das Δ D50 des Rußes 72-90 nm ist und das Δ D50/D-Mode-Verhältnis des Rußes 0,82-1,00 ist.
- 55 9. Kautschuk-Zusammensetzung gemäß Anspruch 7, worin der Kautschuk Naturkautschuk ist.

10. Kautschuk-Zusammensetzung gemäß Anspruch 7, worin der Ruß in einer Menge von 50 bis 100 Gewichtsteilen pro 100 Gewichtsteile Kautschuk vorliegt.

Revendications

- 5 1. Noir de carbone ayant CTAB 120-160m²/g, N₂SA de 125-180m²/g, CDBP de 95-120cc/100g, DBP de 110-145cc/100g, rapport Tint/CTAB de 0,80-1,10, ΔD50 de 70-100 nm et rapport ΔD50/mode D de 0,80-1,05.
- 10 2. Noir de carbone de la revendication 1 où CTAB est de 125-170m²/g, N₂SA est de 125-170m²/g, CDBP est de 98-117cc/100g, DBP est de 112-140 cc/100g, rapport Tint/CTAB de 0,85-1,05, ΔD50 de 72-90 nm et rapport ΔD50/mode D de 0,82-1,00.
- 15 3. Noir de carbone de la revendication 1, où CTAB est de 131m²/g, N₂SA est de 141m²/g, CDBP est de 104cc/100g, DBP est de 118cc/100g, rapport Tint/CTAB de 1,01, ΔD50 de 86 nm et rapport ΔD50/mode D de 0,96.
- 20 4. Noir de carbone de la revendication 1, où CTAB est de 129m²/g, N₂SA est de 133m²/g, CDPB est de 100 cc/100g, DBP est de 114 cc/100g, rapport Tint/CTAB de 1,02, ΔD50 de 78nm et rapport ΔD50/mode D de 0,91.
- 25 5. Noir de carbone de la revendication 1, où CTAB est de 149m²/g, N₂SA est de 159m²/g, CDBP est de 110cc/100g, DBP est de 108 cc/100g, rapport Tint/CTAB de 0,88, ΔD50 de 82nm et rapport ΔD50/mode D de 0,87.
- 30 6. Noir de carbone de la revendication 1, où CTAB est de 135m²/g, N₂SA est de 156m²/g, CDBP est de 102 cc/100g, DBP est de 115 cc/100g, rapport Tint/CTAB est de 1,00, ΔD50 est de 74nm et rapport ΔD50/mode D est de 0,84.
- 35 7. Composition de caoutchouc comprenant 100 parties en poids d'un caoutchouc et 10 à 250 parties en poids d'un noir de carbone ayant CTAB de 120-160m²/g, N₂SA de 125-180m²/g, CDBP de 95-120cc/100g, DBP de 110-145 cc/100g, rapport Tint/CTAB de 0,80-1,10, ΔD50 de 70-100nm et rapport ΔD50/mode D de 0,80-1,05.
- 40 8. Composition de caoutchouc selon la revendication 7, où CTAB du noir de carbone est de 125-150m²/g, N₂SA du noir de carbone est de 125-170m²/g, CDBP du noir de carbone est de 98-117cc/100g, DBP du noir de carbone est de 112-140 cc/100g, le rapport Tint/CTAB du noir de carbone est de 0,85-1,05, ΔD50 du noir de carbone est de 72-90 nm et le rapport ΔD50/mode D du noir de carbone est de 0,82-1,00.
- 45 9. Composition de caoutchouc selon la revendication 7, où le caoutchouc est du caoutchouc naturel.
- 50 10. Composition de caoutchouc de la revendication 7, où le noir de carbone est présent en une quantité de 50 à 100 parties en poids pour 100 parties en poids de caoutchouc.
- 55

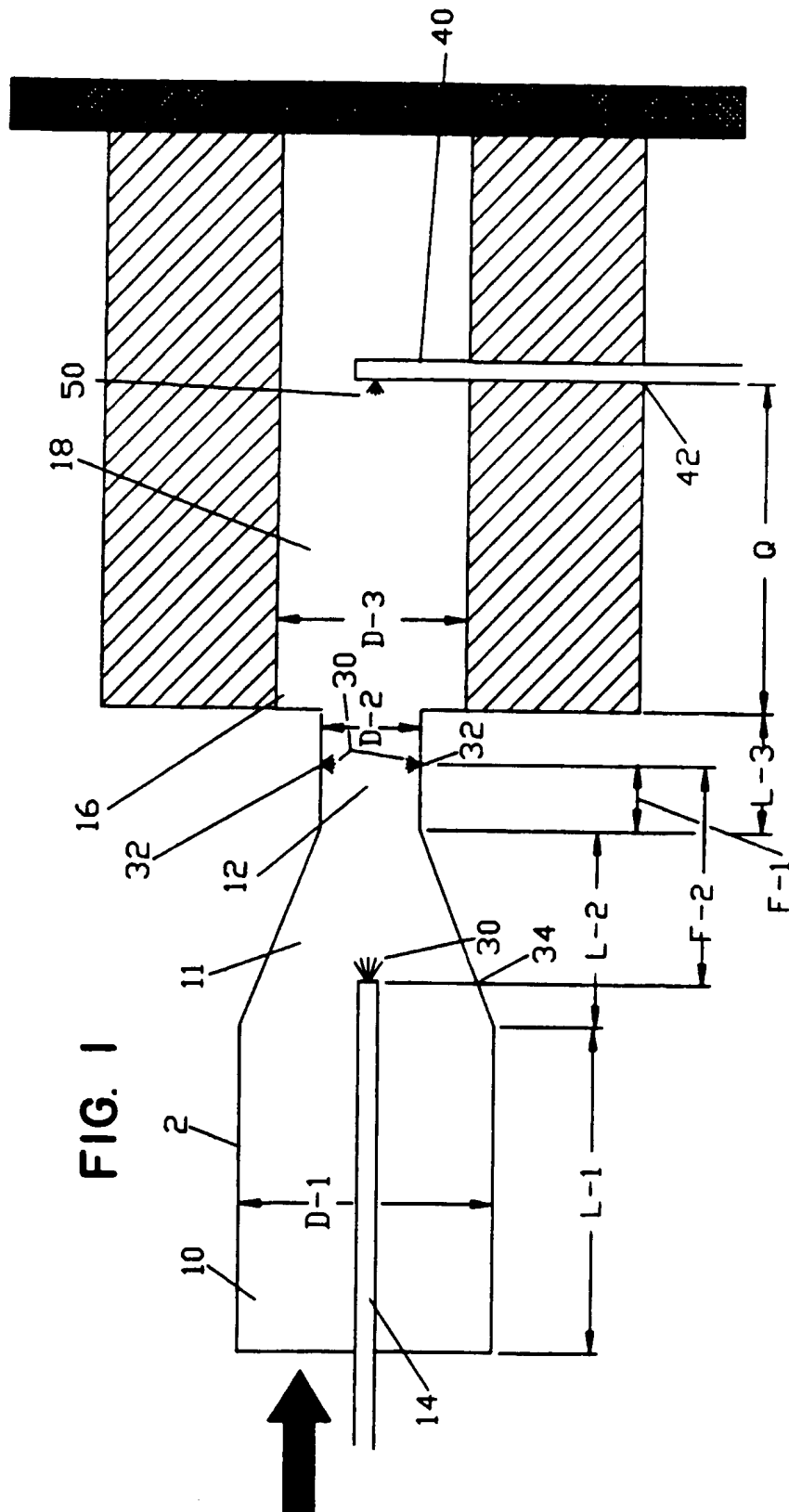


FIG. 2

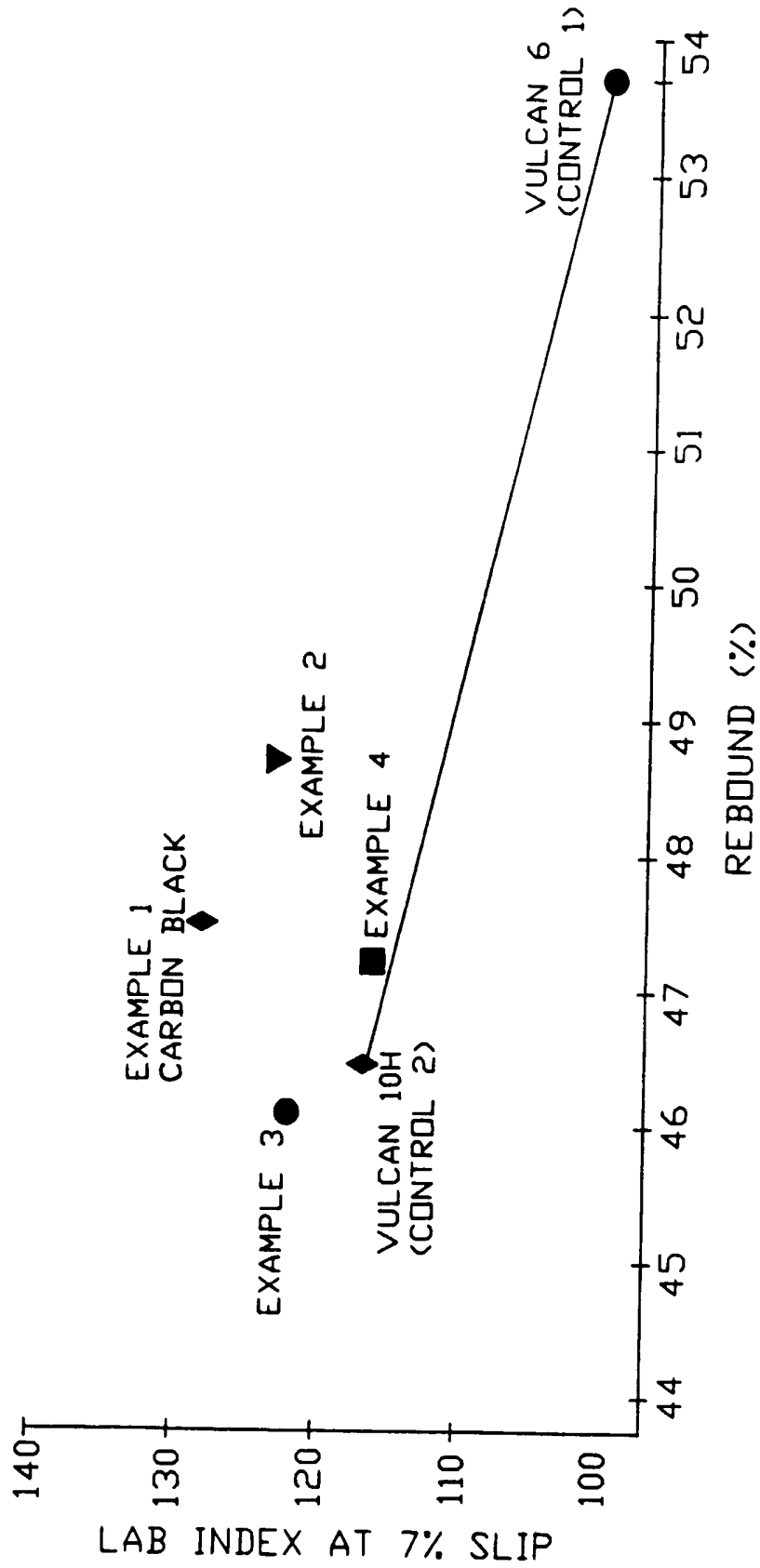


FIG. 3

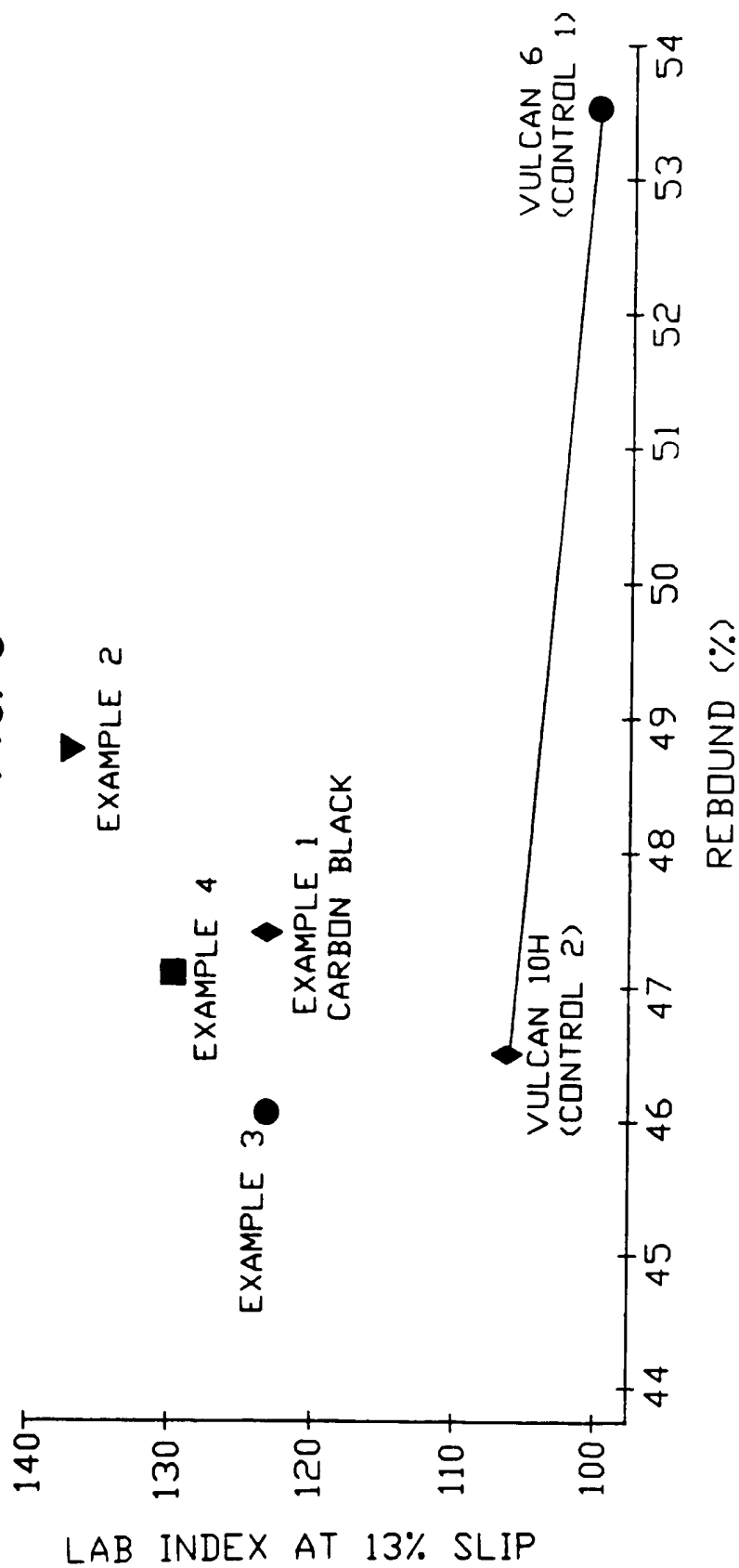
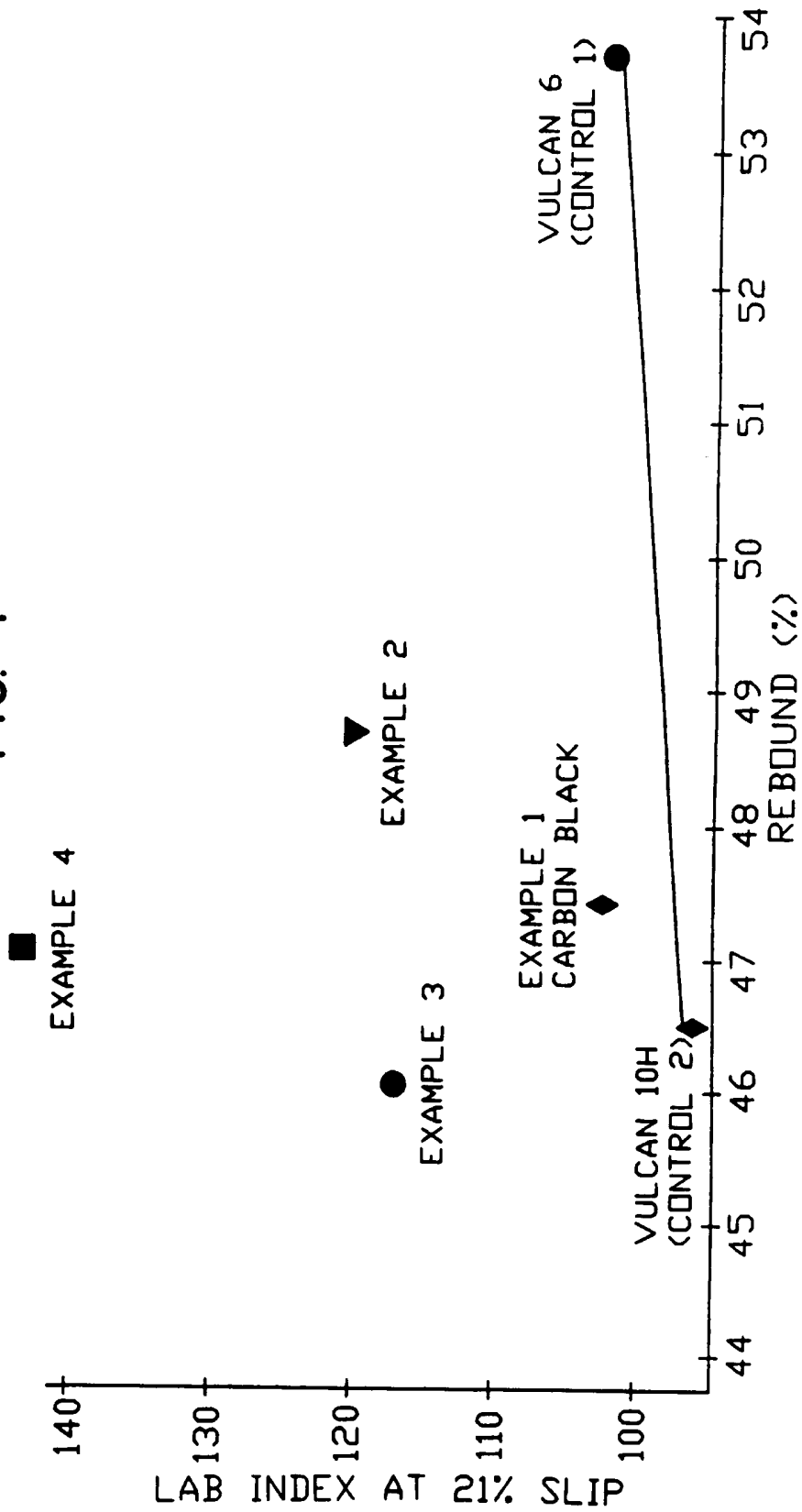


FIG. 4



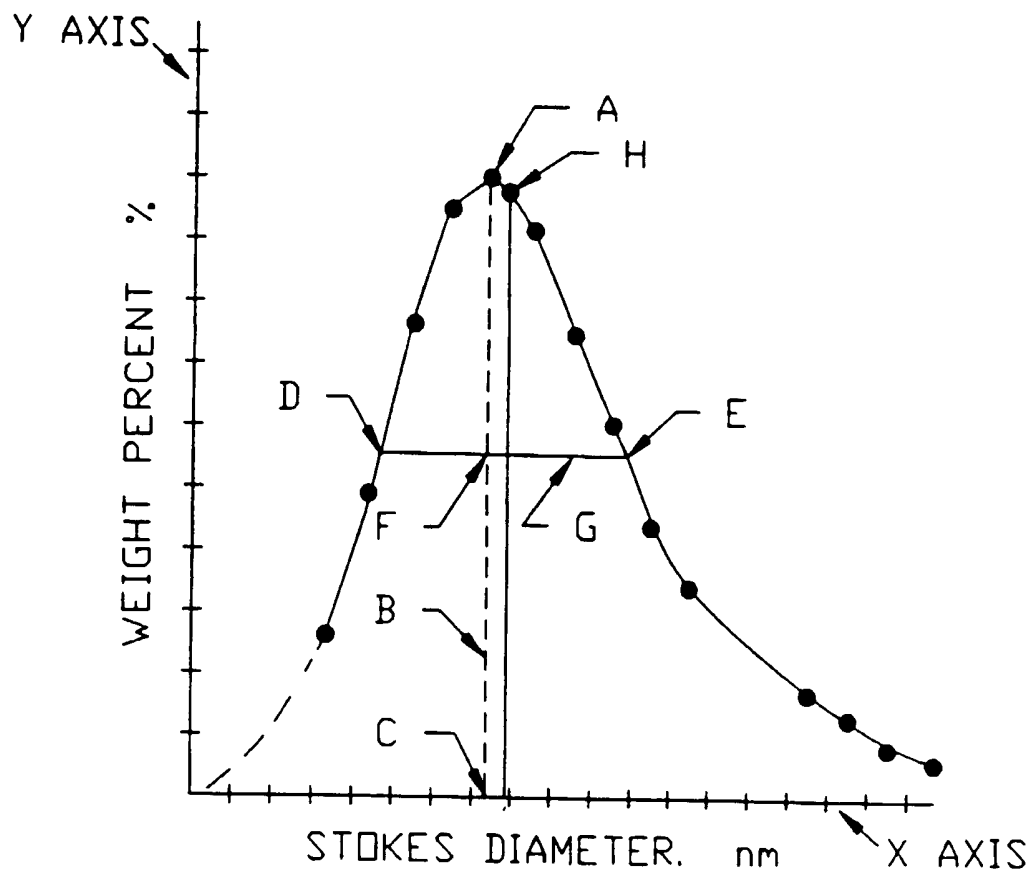


FIG. 5